From the Beginnings of Artificial Cold to Climate-Friendly Fluids; Evolution of Refrigerants Application





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Acknowledgement

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Background

O Refrigeration is used everywhere

Food industry, air conditioning, cryogenics, medicine and health products, energy, etc.

$\,\circ\,$ Use of refrigeration will increase, particularly in developing countries

Use of refrigeration has environmental consequences

- Current refrigerants (HFCs) are greenhouse gases; need for low-GWP refrigerants
- Emissions of CO₂ from fossil fuel power plants; need for high efficiency
- Kigali amendment to the Montreal Protocol (2016); production & consumption of HFCs to be cut by more than 80 % over the next 30 years.

Weighed GWP across all sectors ≈ 300



Industrial revolution (1760~1840)





- Improved productivity through inventions and new production methods (Watt's steam engine; iron production; textile industry)
- Sustained growth of income and population
- The most important event since the domestication of animals and plants (10 000 years ago)

Beginnings of artificial cold

- 1755 apparatus to make ice by evaporation of water at reduced pressure; W. Cullen
- 1824 genesis of thermodynamics; Carnot
- 1834 refrigeration machine using compression of a liquefiable gas; Perkins
- 1834 demonstration of the Peltier effect
 - reliable compressor; Harrison
 - absorption machine; F. Carre
 - air cycle machine; Gorrie
 - machine relying on evaporation of water (R-718) at reduced pressure; E. Carre
 - refrigerants: ethyl ether, methyl ether (R-E170), petrol ether + naphtha (chemogene), CO₂ (R-744), ammonia (R-717), SO₂ (R-764), methyl chloride (R-40)
- 1876 ammonia compressors by Linde; application of thermodynamics

Main applications: ice making, transport of meat by sea, and brewing

- 1890 -> 1900 collapse of ice harvesting
- 1918 dominant refrigerants: ammonia, CO₂, SO₂
- 1920s introduction of HCs
- 1931 introduction of CFC refrigerants

Ice harvesting







Thevenot, R. (1979)



Natural fluids

100.0

-78.4

-194.2

H₂O

CO₂

Whatever

1 st

Generation

1830 - 1930

worked

air

HFO-1234ze(E) # of fluorine atoms R-600a R-717 -33.3 - 11.7 # of hydrogen atoms +1 **R-290** - 42.1 # of carbon atoms -1 # C=C double bounds R-1270 - 47.7 Normal boiling Ammonia point (°C) **Fluorinated fluids** HFCs & HCFC **CFCs & HCFCs HFOs** (Hydrofluoroolefins) alobal safety & ozone warmina 4th Generation 3rd Generation 2nd Generation durability protection mitigation 2010s -1931 – 1990s 1990 - 2010s Water chillers R-1336mzz(Z) 33.4 **R-11 R-123** (HCFC) 27.8 23.7 (centrifugal) R-1233zd(E) -26.1 18.3 **R-134a** Domestic **R-12** -29.8 R-1224yd(Z) 14.6 **R-407C** -43.6 $GWP \leq 2$ refrigeration **R-1234ze(E)** (R-32/125/134a) -19.0 Air **R-410A** -51.4 **R-1234yf** -29.5 **R-22** -40.8 conditioners (R-32/125)Industrial **R-404A** -45.7 **R-502** -45.3 refrigeration (R-125/143a/134a) (R-115/22)

Application of refrigerants

Calm (2008), Calm (2012), Myhre, G. et al. (2013)

H₂O

CO₂

Whatever

1 st

Generation

1830 - 1930

worked

air



Application of refrigerants



NIST search for low-GWP fluids (2012 – 2017)

Objective: Identify molecules that might be good replacements for R-410A and R-22

Air-conditioning and refrigeration applications

- positive displacement compressors
- forced-convection air-to-refrigerant heat exchangers

Approach: Perform <u>screening</u> using <u>comprehensive</u> database

(PubChem lists over 60 million unique chemical structures)

Important attributes/filters:

- Performance: COP, volumetric capacity (Q_{vol})
- Environmental: ODP, GWP
- Safety: toxicity, flammability
- Materials: stability, compatibility (lubricant, seals, metals, etc.)





• Cost

NIST search for low-GWP fluids (cont.)



21 (primary interest) + 3 (commercial interest) + 3 (low τ_{crit}) = 27 fluids

Air conditioning (McLinden et al., 2017)

Refrigeration and heating (Domanski et al., 2017)

Performed detailed simulations with optimized heat exchangers for 24 fluids

New toxicity data on R-1132a; 27 + 1 (low τ_{crit}) \longrightarrow 28 fluids

28 candidate fluids

Basic cycle; air conditioning; optimized heat exchangers

21 fluids of primary interest:

46 °C < T_{cr} < 146 °C Q_{vol} > 0.33 $Q_{vol,R-410A}$

15 - at least mildly flammable6 - unknown hazards

7 additional fluids:

- subcritical operation; 3 fluids
 [R-134, R-1123, R-1225ye(Z)]
- supercritical or near-critical operation; 4 fluids
 [R-170, R-41, R-1132a, R-744]



			GWP	T _{cr}	СОР	Q vol
Hvdrocarbons and dimethylether				(К)	COP _{R410A}	Q vol, R410A
ethane	CH ₃ -CH ₃	R-170	6	305.3		-
propene (propylene)	CH ₂ =CH-CH ₃	R-1270	2	364.2	1.033	0.689
propane	CH ₃ -CH ₂ -CH ₃	R-290	3	369.9	1.014	0.571
methoxymethane (dimethylether)	CH ₃ -O-CH ₃	R-E170	1	400.4	0.996	0.392
cyclopropane	-CH2-CH2-CH2-	R-C270	86	398.3	1.018	0.472
Fluorinated alkanes (HFCs)						
fluoromethane	CH ₃ F	R-4 1	116	317.3		
difluoromethane	CH_2F_2	R-32	677	351.3	1.038	1.084
fluoroethane	CH ₂ F-CH ₃	R-161	4	375.3	1.026	0.601
1,1-difluoroethane	CHF ₂ -CH ₃	R-152a	138	386.4	0.981	0.399
1,1,2,2-tetrafluoroethane	CHF ₂ -CHF ₂	R-134	1120	391.8	0.967	0.348
Fluorinated alkenes (HFOs) and alky	nes					
1-1-difluoroethene	CF ₂ =CH ₂	R -1132a	<1	324.2		
fluoroethene	CHF=CH ₂	R-1141	<1	327.1	0.968	1.346
1,1,2-trifluoroethene	CF ₂ =CHF	R-1123	3	343.0	0.956	1.054
3,3,3-trifluoroprop-1-yne	CF3-C≡CH	n.a.	1.4	363.3	0.988	0.545
2,3,3,3-tetrafluoroprop-1-ene	CH ₂ =CF-CF ₃	R-1234yf	<1	367.9	0.954	0.414
(E)-1,2-difluoroethene	CHF=CHF	R-1132(E)	1	370.5	1.016	0.591
3,3,3-trifluoroprop-1-ene	CH ₂ =CH-CF ₃	R-1243zf	<1	376.9	0.964	0.372
1,2-difluoroprop-1-ene‡	CHF=CF-CH ₃	R-1252ye‡	2	380.7	0.973	0.355
(E)-1,3,3,3-tetrafluoroprop-1-ene	CHF=CH-CF ₃	R-1234ze(E)	<1	382.5	0.939	0.320
(Z)-1,2,3,3,3-pentafluoro-1-propene	CHF=CF-CF ₃	R-1225ye(Z)	<1	384.0	0.922	0.273
1-fluoroprop-1-ene‡	CHF=CH-CH ₃	R-1261ze‡	1	390.7	0.975	0.353
Fluorinated oxygenates						
trifluoro(methoxy)methane	CF ₃ -O-CH ₃	R-E143a	523	377.9	0.957	0.366
2,2,4,5-tetrafluoro-1,3-dioxole	-O-CF ₂ -O-CF=CF-	n.a.	1	400.0	0.936	0.337
Fluorinated nitrogen and sulfur com	pounds					
N,N,1,1-tetrafluormethaneamine	CHF ₂ -NF ₂	n.a.	20	341.6	0.965	0.807
difluoromethanethiol	CHF ₂ -SH	n.a.	1	373.0	1.010	0.582
trifluoromethanethiol	CF ₃ -SH	n.a.	1	376.2	0.977	0.418
Inorganic compounds		_				
carbon dioxide	CO ₂	R-744	1.00	304.1		
ammonia	NH ₃	R-717	<1	405.4	1.055	0.746

0



COP and **Q**_{vol}; air conditioning





COP and *Q*_{vol}; air conditioning







COP and *Q*_{vol}; air conditioning







Ideal cycle simulations



Basic cycle

EVAPORATOR

Why there are no low-GWP fluids that are nonflammable and have high Q_{vol}?

Trade-off between low GWP and flammability

GWP can be lowered by:

Replacing F or Cl with H. \bigcirc It shortens the atmospheric life but leads to flammability.





R-134a GWP = 1300; T_{cr} = 101.1 °C Class: 1



Class: 2L

R-152a GWP = 138; T_{cr} = 113.3 °C Class: 2

Adding a C=C double bond. Contributes to the reaction with oxygen.





GWP = 4800; T_{cr} = 72.7 °C

R-1225ye(Z) GWP < 1; T_{cr} = 110.9 °C Class: 1

Is it all ? Why some other fluids did not make it ?

- Peroxides [-O-O-]: unstable, one dropped
- \circ Alkynes [-C=C-]: = generally less stable than =, one retained
- Ketenes [>C=C=O]: generally very reactive, three dropped
- o Allenes [>C=C=C<]: very reactive</p>
- Alcohols [-OH]: high T_{cr}



- \circ = CF₂ group: high reactivity often associated with toxic effects; some exceptions
- = OF group: not stable, may lead to hydrofluoric acid

How reliable was the screening process?

Did we miss good fluids?

PubChem database is complete (?)

PubChem lists 30 three-carbon HFOs out of 31 possible. It is unlikely that the missing molecule would posses significantly different properties than those already listed.

Component atoms: only C, H, N, O, S, F, Cl, Br (?) Maximum number of atoms: 18 (?)

Additional screening of a different database with 2000 industrial fluids yielded small molecules with the above eight elements only.

- GWP₁₀₀ < 1000 (?)
- Critical temperature: $46 \degree C < T_{cr} < 146 \degree C$ (?) Estimated with standard deviation of 16.5 K (4.5 %). $T_{cr, R-410A}$ =71.3 °C
- Stability and toxicity (?)

Published data, which may be erroneous. E.g., toxicity of R-1132a Unstable fluid may be stabilized and used in the system. E.g., R-1123, R-13I1 (CF_3I)





CF₃I - **ASHRAE Standard 34 proposed addenda 't' and 's'**

Addendum 't'

R-13I1

```
Chemical name = trifluoroiodomethane
Chemical formula CF<sub>3</sub>I
```

- OEL = 500 ppm v/v
- Safety Group = A1
- GPW = 0.4

Addendum 's'

```
R-466A
Composition (mass %) = R-32/125/13I1
(49/11.5/39.5)
OEL = 860 ppm v/v
Safety Group = A1
GWP = 733
```

• ODP = 0.008

- Good thermodynamic properties
- Fire suppression properties
- Toxicity of CF₃I was studied in the 1990s (McCain and Macko, 1999).
 CF₃I is SNAP-approved fire suppressing agent replacing halon 1301 (total flooding) and halon 1211 (streaming), with restrictions to unoccupied and non-residential uses, respectively.

 $\mathbf{F} - \mathbf{\dot{C}} - \mathbf{\dot{F}}$

R-1234yf/CF₃I (70/30) was studied in the 2000s for automotive ACs, within the Cooperative Research Program CRP150 (SAE).
 Dropped over concerns related to the non-zero ODP and reactivity of CF₃I. (Brown, 2012)

 $CF_{3}I$ is expected to see future application as a component of <u>nonflammable</u> blends. Application challenge: reactivity

Normalized Flammability Index $\overline{\Pi}$

Novel empirical flammability estimate

- Uses F/(F+H) in reactants and adiabatic flame temperature T_{ad}
- Effects of humidity are included
- Based on the ASHRAE Std. 34 experimental database of refrigerant flammability



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Flammability index

$$\Pi = \arctan \left(\frac{T_{ad} - 1600}{2500 - 1600}, \frac{F}{F + H}\right) \cdot \left(\frac{180}{\pi}\right)$$

 Π 1,2L = 36; flammability boundary between classes 1 and 2L

Normalized flammability index

$$\overline{\Pi} = \frac{\Pi - \Pi_{1,2L}}{90 - \Pi_{1,2L}} \cdot 100$$

 $\overline{\Pi} < 0$ No flame propagation

Linteris et al. (2017)



Initial temperature = 60 °C; mole fraction of H_2O in air = 0.014

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Search for nonflammable replacements for R-134a

- Comprehensive evaluation binary, ternary and four-component blends (13 compounds considered)
- \circ Selection criteria:
 - Minimize flammability
 - Minimize GWP
 - Maximize COP
 - Match volumetric capacity to that of R-134a



Blend	Composition		СОР	Q	Π
components	(molar)	GVVP	COP _{R-134a}	Q _{R-134a}	
R-152a/1234yf	0.08/0.92	8	0.980	0.957	7.7
R-134a/1234yf	0.20/0.80	238	0.980	0.996	2.8
R-134a/152a/1234yf	0.20/0.16/0.64	270	0.987	0.984	8.7
R-152a/1234yf/134	0.16/0.48/0.36	417	0.984	0.900	7.5
R-134a/1234yf	0.36/0.64	436	0.985	1.018	1.0
R-134a/1234yf/1243zf	0.36/0.44/0.20	451	0.988	1.004	5.2
R-134a/152a/1234yf	0.36/0.20/0.44	496	0.994	0.994	8.3
R-134a/1234yf	0.44/0.56	537	0.987	1.025	-0.1
R-134a/1234yf	0.468/0.532 *	573	0.988	1.027	-0.4
R-134a/1234yf/134	0.48/0.48/0.04	633	0.987	0.975	-1.1
R-134a/1234yf/1234ze(E) 0.52/0.32/0.16	640	0.987	0.989	-1.2
R-134a/1234yf	0.52/0.48	640	0.989	1.029	-1.2
R-134a/1234yf/134	0.4/0.44/0.16	665	0.986	0.958	-1.3
R-134a/125/1234yf	0.44/0.04/0.52	676	0.985	1.049	-1.5
R-134a/227ea/1234yf	0.40/0.04/0.56	681	0.984	1.007	-1.5
R-134a/1234ze(E)	0.60/0.40	745	0.988	0.908	-2.4
R-134a/1234yf	0.60/0.40	745	0.990	1.031	-2.4
R-134a/1234ze(E)/1243z	f 0.60/0.36/0.04	750	0.990	0.966	-1.5
R-134a/1234yf/1234ze(E) 0.64/0.2/0.16	799	0.990	0.986	-3.0
R-134a/152a/1234yf	0.64/0.04/0.32	817	0.993	1.023	-1.8
R-134a/1234yf/134	0.52/0.32/0.16	824	0.990	0.966	-3.2
R-134a/1234ze(E)	0.68/0.32	852	0.991	0.929	-3.7
R-134a/1234yf/1243zf	0.68/0.2/0.12	870	0.994	1.020	-1.1

⁺ R-513A





Calm (2008), Calm (2012), Myhre, G. et al. (2013)

* Source other than IPCC AR5 ${}^{(1)}$ R-1336mzz(Z)/1130(E) (74.7/25.3) ${}^{(2)}$ R-1234yf/134a (56/44)



Calm (2008), Calm (2012), Myhre, G. et al. (2013)

* Source other than IPCC AR5 ⁽¹⁾R-1234yf/134a (56/44)





Cooling technologies

sorted by primary energy input

Acceptance criteria

- Coefficient of Performance
- Environmental
- Safety
- Cost
- Reliability
- Serviceability
- Physical size, weight

Best prospects for competing with vapor compression





Food refrigeration



Concluding comments



Availability of low-GWP refrigerants varies between applications

- Good availability of low-pressure fluids (low GWP, nonflammable)
- No direct HFO replacement candidate for R-22 or R-410A
 Single-component medium- and high-pressure replacement fluids are at least mildly flammable

• Prospects for finding new viable refrigerants are minimal.

New equipment will have to be designed using the fluids we know already and their blends.

• Trade off between GWP and flammability

Concluding comments



• Alternative cooling technologies?

Alternative technologies will gain entry in niche applications

<u>but</u>

will need significant development effort and

material breakthroughs to be competitive and enter the main stream.

• We will have to use refrigerants judiciously, which includes:

- Selection of refrigerant for each application recognizing environmental and safety considerations
- High-efficiency, leak-free equipment
- Improved refrigerant handling practices (equipment commissioning, servicing, and decommissioning).





Thank you for your attention.

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