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#### Air Conditioning in High Ambient temperatures. Comparisons of Alternative Fluids.

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### **Outline/Agenda**

- General presentation of fluids for A/C (chillers and D-X).
  - Why blends versus pure fluids ?
  - Fluids in the study.
  - Behavior of blends.
  - ce on Compressors and • "Constant LMTD Analysis" for zeotropic blends.
  - Comparisons of COP and Volumetric capacity.
- Focus on alternatives to R-22 and R-410A
  - Zoom on these alternatives
  - Correction for COP of fluids depending on their capacity in retrofit tests.
- Conclusions.



#### Acknowledgement

The paper presented is a slightly amended version of an article presented at the *"Second International Conference on Energy and Indoor Environment for Hot Climates"* organized by ASHRAE and Qatar University in Doha, Qatar, February 26 and 27, 2017. The initial paper is reproduced with kind permission of ASHRAE - Copyright 2017 ASHRAE.



### **Outline/Agenda**

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  - Why blends versus pure fluids ?
- • Focus on alternatives to R-22 and R-410A
  - these alternatives
  - Correction for COP of fluids depending on their capacity in retrofit tests.
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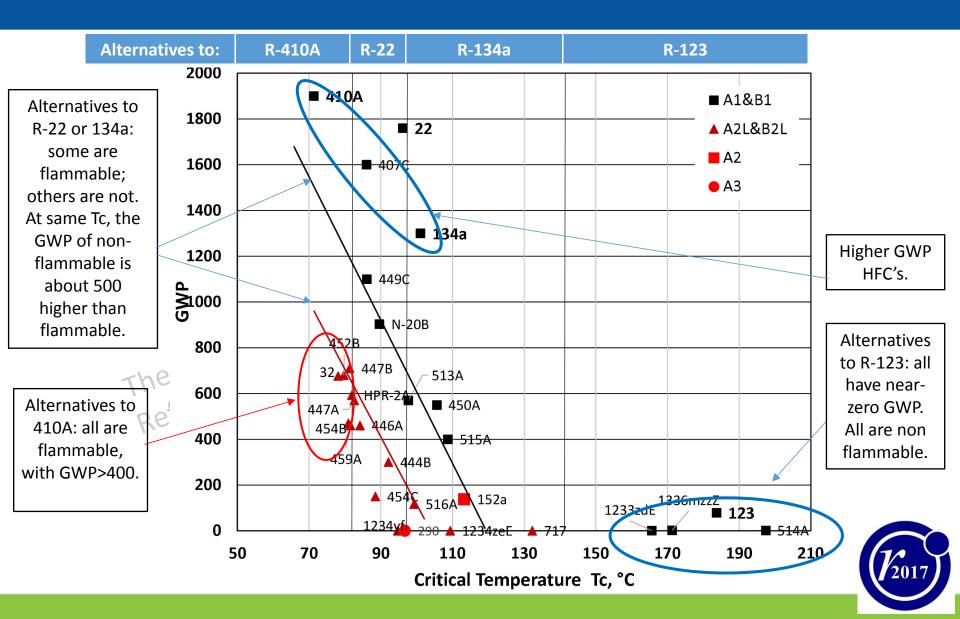


### **Context and purposes**

- Four "benchmark" fluids are currently used in A/C (Chillers and D-X): R-123, R-134a, R-22 and R-410A.
- The phase-out of R-123 and R-22 is completed in "developed countries", and ongoing in Art-5 countries.
- Lower GWP alternatives to R-134a and R-410A are desired.
- So, alternatives are being investigated for all the fluids currently used in A/C.
- One of the proposed alternatives (R-290) is highly flammable; many others alternatives have lower flammability ("2-L" class)
- It is agreed that alternative solutions should not result in lower energy efficiency.
- The quest for alternatives results in a trade-offs between flammability, GWP, energy efficiency and cost.
- A purpose of this presentation is to shed light of some of these trade-offs.



#### An Overview of the Fluids



#### More details on the fluids

The alternatives to the base line fluids are ranked by Critical Temperature.

Higher Critical Temperature tends to lower pressure and capacity.

Alternatives blends to 410A have moderate glide (I.3 to 4.2 K)

Alternatives blends to R-22 have higher glide (4.5 to 7.7 K)

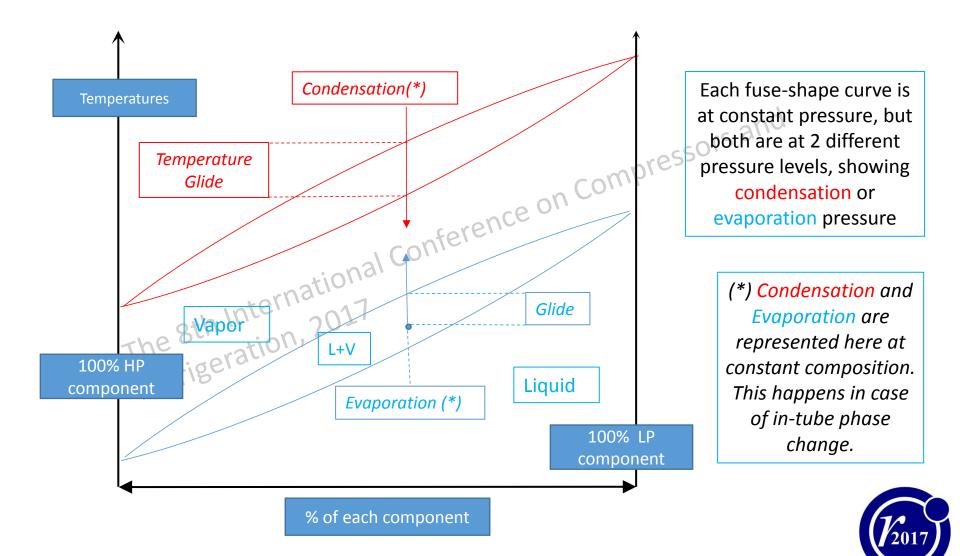
Alternatives to 134a and 123 have little (<0.6 K) or no glide.

	Crit Refrigerant		ical				N1º.	At 40°C	(104°F)	GWP	Safety
	Tempe		rature	A	ternativ	e to K-	IN :	Pressure	Glide	100	class
	R-N°	°C	۴F	123	134a	22	410A	Bar-a	к	(AR5)	\
	125	66.0	151				0	20.1	/	3170	A1
	410A	71.3	160				0	24.2	0.1	1900	A1
	32	78.1	173				$\checkmark$	24.8	/	677	A2L
	452B	79.7	175				$\checkmark$	22.6	1.3	680	A2L
	454B	80.9	178				$\checkmark$	22.3	1.5	470	A2L
	447B	81.3	178				$\checkmark$	21.4	3.9	710	A2L
	459A	81.5	179				$\checkmark$	21.9	2.0	461	A2L
	HPR-2A	81.9	179				$\checkmark$	21.7	3.0	593	A2L
	447A	82.6	181				$\checkmark$	20.8	3.9	570	A2L
	446A	84.2	184				$\checkmark$	20.7	4.2	460	A2L
	407C	86.0	187			0		16.4	5.0	1600	A1
	449C	86.1	187					16.3	4.6	1100	A1
	454C	88.5	191					15.6	6.3	150	A2L
	N-20B	89.6	193					14.5	4.5	904	A1
~	444B	92.1	198					15.9	7.7	300	A2L
9	1234yf	94.7	202		$\sim$			10.2	/	<1	A2L
	22	96.1	205			0		15.3	/	1760	A1
	290	96.7	206			$\checkmark$		13.7	1	0	A3
1	513A	97.7	208		$\checkmark$			10.7	1	570	A1
	516A	99.3	211		$\checkmark$			10.5	0.0	131	A2L
	134a	101	214		0			10.2	/	1300	A1
	227ea	102	215		0			7.0	1	3350	A1
	450A	106	222		$\checkmark$			8.9	0.6	550	A1
	515A	109	228		$\checkmark$			7.6	/	400	A1
	1234zeE	109	229		$\checkmark$			7.7	/	<1	A2L
	152a	113	236		$\checkmark$			9.1	/	138	A2
	717	132	270					15.6	/	0	B2L
	1233zdE	166	330	$\checkmark$				2.2	/	1	A1
	1336mzzZ	171	340	$\checkmark$				1.3	1	2	A1
	123	184	363	0				1.5	/	79	B1
	514A	197	387	$\checkmark$		·		1.5	1	1.7	B1

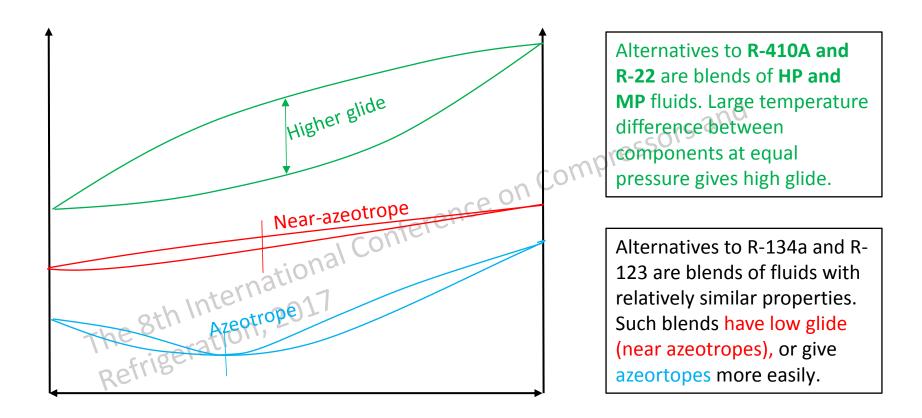
### Why are blends proposed?

- For each of the base line fluids (R-123, R-134a, R-22, R-410A), the idea is to find alternatives with relatively similar capacity.
- To replace R-22, the only pure compounds with "similar" cooling capacity are Ammonia (R-717) and Propane (R-290).
- Ammonia is toxic, and as of today, it is not suitable for D-X systems (material compatibility and high discharge temperature).
- R-290 is highly flammable.
- No other applicable pure compound has similar cooling capacity.
- Blends to replace R-22 are using a combination of:
  - 2 fluids with higher pressure and capacity:R-125 and R-32.
  - 3 fluids with lower pressure / capacity: R-134a, and the HFO's R-1234ze and yf.
  - Plus occasionally small amount of other fluids: R-152a and R-227ea (close to 134); R-290.

### Non-azeotrip, 2 components blend



### **Different blend behaviors**



**Reminder**: - A pure fluid or azeotropic blend has no temperature glide.

- A zeotropic (or non-azeotropic) blend has some glide.
- A near-azeotrope (or quasi-azeotrope) has very low glide (e.g. R-410A)

#### **Composition of the blends / Pressures**

Ref.	Brand	ASHRAE			Comp	ositions	by mass			Glide (K)	Safety	GWP 100
fluid	name	R-N°	R32	R125	134a	1234yf	1234ze	C	Others	@ 40°C	class	(AR-5)
		410A	50	50						0.12	A1	1900
	DR-5A	454B	68.9			31.1				1.53	A2L	470
	DR-55	452B	67	7		26				1.34	A2L	680
R-410A	L-41-1	446A	68				29	R-	290, 3%	4.19	A2L	460
K-410A	L-41-2	447A	68	3.5			28.5			3.94	A2L	570
	ARM-71A	459A	68			26	6			2.04	A2L	461
	L41z	447B	68	8			24		mp	3.43	A2L	710
	HPR-2A	/	76		6		18	S	,0,	2.97	A2L	593
	L-20A	444B	41.5				48.5	R-1	52a, 10%	7.71	A2L	300
	N-20B	/	13	13	31	43				4.54	A1	904
R-22		407C	23	25	52	// -				5.00	A1	1600
	DR-3	454C	21.5	ona		78.5				6.29	A2L	150
	DR-93	449C	20	20	29	31				4.62	A1	1100
	XP10	513A	2	h11	44	56				0.00	A1	570
D 1245	N-13	450A	n, L		42		58			0.63	A1	550
R-134a	HDR115	515A					88	R-22	27ea, 12%	0.00	A1	400
	ARM-42	516A			8.5	77.5		R-1	52a, 14%	0.01	A2L	131
R-123	<b>R-123</b> DR-10 514A					1336r	nzz, 74.7%	; R-11	.30E, 25.3%	0.00	B1	1.7
Press	Pressure color code:			Mediu	m-High	2	3					
	Iternative		High R-410A		22	R-134a	R-123		Alternat	ives to 13	4a	Alternat
								_	are blen	ds of <b>only</b>	/ MP	blend to
								1 1	<b>.</b>		.	

Alternatives to **R-410A** and **R-22** are blends of **HP and MP** fluids. Alternatives to **410A** have more HP components and less MP than alternatives to R-22. Alternatives to **134a** are blends of **only MP** fluids (134a, HFO's 1234yf or ze, 227ea; 152a). Alternative blend to **R-123** is a blend of LP fluids.

#### **Composition of the blends / Flammability**

	Ref.	Brand	ASHRAE		Compositions by mass			Glide (K)	Safety	<b>GWP 100</b>		
	fluid	name	R-N°	R32	R125	134a	1234yf	1234ze	Others	@ 40°C	class	(AR-5)
All the			410A	50	50					0.12	A1	1900
alternatives		DR-5A	454B	68.9			31.1			1.53	A2L	470
to 410A are		DR-55	452B	67	7		26			1.34	A2L	680
flammable.	R-410A	L-41-1	446A	68				29	R-290, 3%	4.19	A2L	460
	R-410A	L-41-2	447A	68	3.5			28.5		3.94	A2L	570
		ARM-71A	459A	68			26	6		2.04	A2L	461
Some		L41z	447B	68	8			24		3.43	A2L	710
alternatives to R-22 or		HPR-2A	/	76		6		18		2.97	A2L	593
134a are		L-20A	444B	41.5				48.5	R-152a, 10%	7.71	A2L	300
flammable.		N-20B	/	13	13	31	43			4.54	A1	904
Some others	R-22		407C	23	25	52				5.00	A1	1600
are not.		DR-3	454C	21.5			78.5			6.29	A2L	150
	-1	DR-93	449C	20	20	29	31			4.62	<mark>A</mark> 1	1100
		XP10	513A			44	56			0.00	A1	570
None of the	D 124	N-13	450A			42		58		0.63	A1	550
alternatives to R-123 is	R-134a	HDR115	515A					88	R-227ea, 12%	0.00	A1	400
flammable.		ARM-42	516A			8.5	77.5		R-152a, 14%	0.01	A2L	131
	R-123	DR-10	514A				1336	mzz, 74.7%	6; R-1130E, 25.3%	0.00	B1	1.7
	-											

3

Flammability color code: 1 2L 2

Higher content of flammable components

 $\rightarrow$  higher flammability of the blend.

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		Ref.	Brand	ASHRAE		Compositions by mass			Glide (K)	Safety	GWP 100		
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to 410A are			DR-55	452B	67	7		26			1.34	A2L	680
flammable.		D /10A	L-41-1	446A	68				29	R-290, 3%	4.19	A2L	460
		R-410A	L-41-2	447A	68	3.5			28.5		3.94	A2L	570
			ARM-71A	459A	68			26	6		2.04	A2L	461
Some			L41z	447B	68	8			24		3.43	A2L	710
alternatives to R-22 or			HPR-2A	/	76		6		18		2.97	A2L	593
134a are			L-20A	444B	41.5				48.5	R-152a, 10%	7.71	A2L	300
flammable.			N-20B	/	13	13	31	43			4.54	A1	904
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	-1		DR-93	449C	20	20	29	31			4.62	A1	1100
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to R-123 is		R-134a	HDR115	515A					88	R-227ea, 12%	0.00	A1	400
flammable.			ARM-42	516A			8.5	77.5		R-152a, 14%	0.01	A2L	131
nammable.		R-123	DR-10	514A				1336	mzz, 74.7%	ն ; R-1130E, 25.3%	0.00	B1	1.7
	Ē												

Flammability color code: 1 2L 2

Higher content of flammable components

 $\rightarrow$  higher flammability of the blend.

Illustrated above in red « box ».

#### Methodology for performance comparisons

- Choose a « base line » unit: the mini-split 410A unit tested under AREP / ORNL programs.
- Start from detailed test results at AHRI-A: capacity, evaporation & condensation, liquid subcooling etc.
- Simulate the same unit with different fluids at same capacity and conditions, assuming same air side conditions (air flow and temperatures in/out), heat transfer and constant compressor efficiency (80%).
- In the case of blend with glide, do it with both exchangers being simultaneously counter-flow (« Cf-Cf ») or parallel flow (« Pf-Pf »).
- To simulate the blends, use the "Constant LMTD" method.



# The "Constant LMTD" Method (1)

- Basic formula:
  - Q = thermal power (evaporator or condenser):

- K = overall heat transfer coefficient, Compressors and
  LMTD = Mean Logarithmic T and the second second
- Assume:
  - Constant capacity Q
  - Same heat transfer area
    - Same heat transfer coefficients
- Then, **LMTD must be the same**, irrespective of:
  - The fluid (even if blend with glide)
  - The arrangement of the exchangers (Counter or Parallel flow).



# The "Constant LMTD" Method (2)

- For the « base line » unit, calculate the LMTD of each exchanger from R-410A test data:
  - Evaporation and condensation temperatures,
  - Air temperatures in/out of evaporator / condenser
- To identify the evaporation pressure with a blend:
  - Assume a temperature for beginning of evaporation.
  - From the glide, calculate the temperature at end of evaporation.
  - Combining with the air temperatures in a given configuration (parallel or counter-flow), calculate the corresponding LMTD.
  - Iterate until this LMTD = LMTD with 410A
- Do the same for the condenser.
- Proceed with cycle calculation using these data

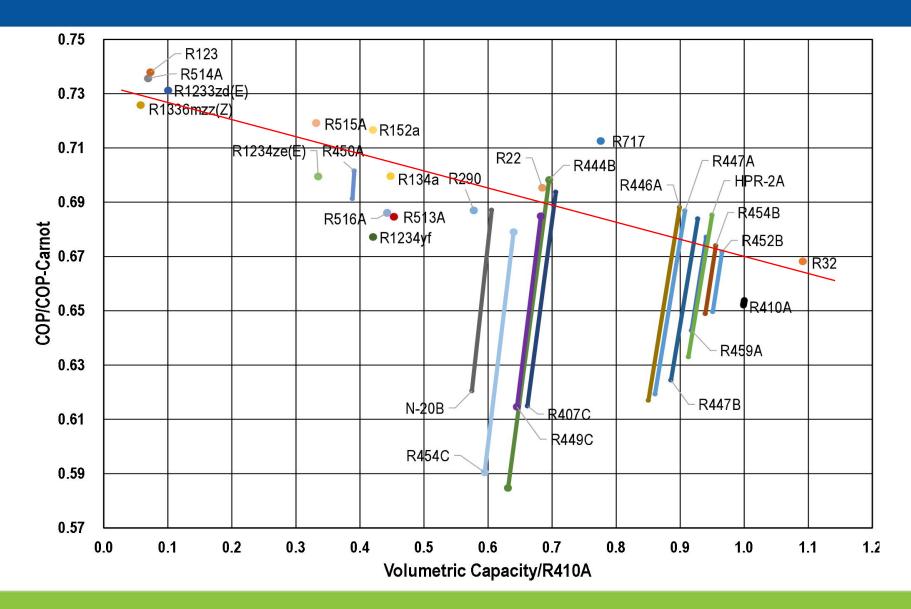


# The "Constant LMTD" Method (3)

- • For various fluids, graph shows COP versus volumetric capacity.
- A « Pure » fluid is represented by a single point.
- A zoetropic blend is represented by a segment between the « Cf-Cf » and « Pf-Pf ».



#### **Performance comparisons results**



### Comments on results (@ AHRI-A)

- In general, fluids with lower Tc / higher pressure have higher capacity but lower COP. General trend, with some variations. Tradeoff between Capacity and COP.
- In the optimum configuration, blends with glide can have slightly better COP at equivalent capacity. But the performance can also be much lower in the arrangement of heat exchangers is not optimum.
- Zeotropic blends are generally not recommended for heat exchanger with shell and tube exchangers and out-of-tube evaporation or condensation (e.g. flooded evaporators).
- Real designs should be close to optimum, but optimization is not necessarily simple. Example: most current designs of small split A/C units have cross flow evaporator.



### **Outline/Agenda**

- General presentation of fluids for A/C (chillers and D-X).
  - Why blends versus pure fluids ?
- • Focus on alternatives to R-22 and R-410A
  - Zoom on these alternatives
  - Correction for COP of fluids depending on their capacity in retrofit tests.
- Conclusions.



### The context

- A/C in HAT will be critical for successful implementation of the Kigali agreement.
- Several research programs are ongoing: AREP, DOE Wealth of data available, butce on compresso
  Detailed recult
- - Detailed results from PRAHA and EGYPRA are confidential.
  - Details from AREP and ORNL are public. But they are results from retrofits. So, alternatives to R-410A and to R-22 are analyzed in 2 separate « boxes », without cross comparison.
  - Units tested are not the same for R-22 and R-410A: Differences in capacity, size of exchangers, compressors etc.
  - Many of the alternatives are blends with glide, which are complex to model by cycle calculations.



### Fluids in the study

Now restricted to fluids proposed as replacements to R-22 and 410A for A/C D-X systems in the AREP program.

Alternatives to R-410A								
Fluid	Brand	Glide @ 40°C						
R-N°	Name	К	°Rae					
32	/	and/C	011					
452B	DR-55	1.3	2.4					
454B 81	DR-5A 2	1.5	2.8					
447B	er 241z	3.4	6.2					
459A	ARM-71A	2.0	3.7					
/	HPR-2A	3.0	5.3					
447A	L-41-2	3.0	5.3					
446A	L-41-1	4.2	7.5					

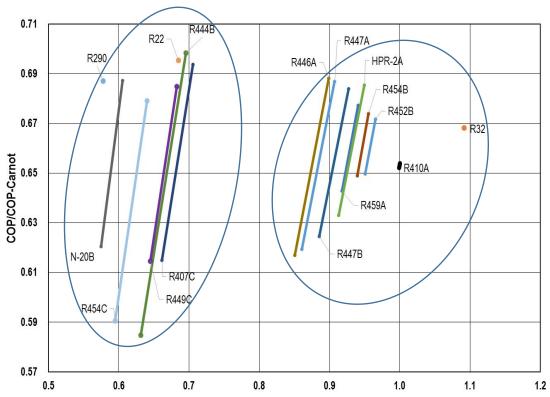
Alternatives to R-22									
Fluid	Brand	Glide @ 40°C							
R-N°	Name	lame K							
407C	/	5.0	9.0						
449C	DR-93	4.6	8.3						
454C	DR-3	6.3	11.3						
/	N-20B	4.5	8.2						
444B	L-20A	7.7	13.9						
290	/	/	/						

and



### Comments on results (AHRI-A / 35°C)

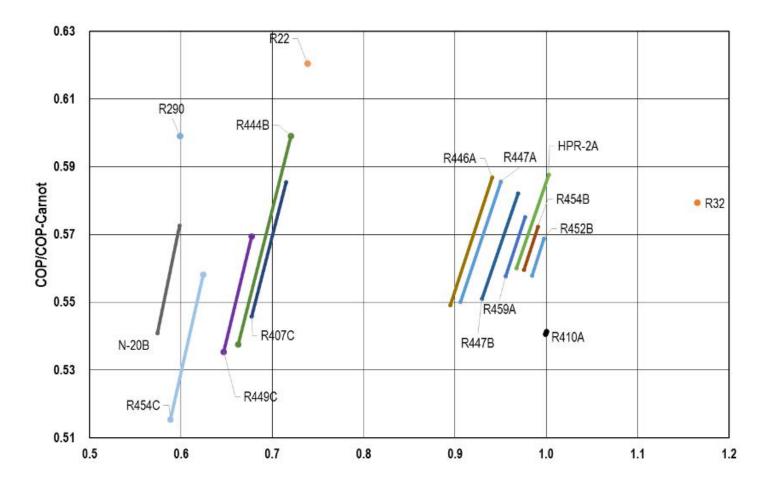
- In the best configuration ("Cf-Cf"), blends can have same or slightly better COP than "pure" fluids.
- But can be much lower if system is not optimized.
- Real designs should be close to optimum, but optimization is not necessarily simple. Example: most current designs have cross flow evaporator.
- Except R-32, all the alternatives to 410A have lower capacity than 410A. All have a better COP.



- Alternatives to R-22 have equivalent or lower capacity than R-22. None of them matches the COP of R-22.
- Even R-290 has a lower calculated COP than R-22. Paradox to be commented later.



#### **Results at High Ambient Temperature (52°C)**



Assumes: Design for same capacity and same indoor conditions as @ AHRI-A



# **Correction for cooling capacity (1)**

- In test data as published (AREP & ORNL reports), capacity and COP are shown "as measured".
- But in retrofits, a lower capacity results in lower temperature differences at the exchangersors
- At the condenser, there is a double effect: at constant • The "SD" is smaller Conferent

  - The leaving air temperature is lower.
- This "artificially" improves the COP.
- Vice-versa, a higher capacity penalizes the COP.
- For "apple to apple" comparisons between fluids, this effect can be corrected.



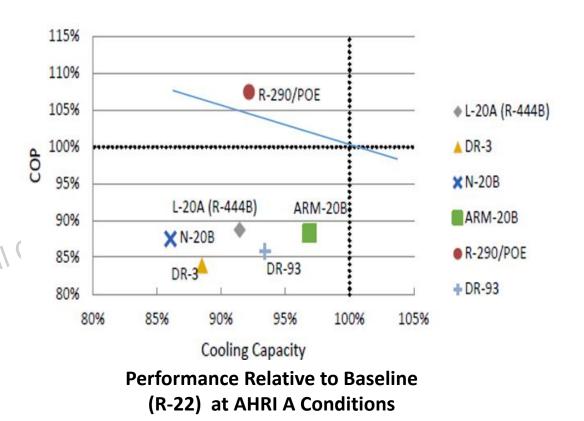
# **Correction for cooling capacity (2)**

- To account for the differences in cooling capacity, start from measured data with a reference fluid (e.g. R-22).
- With a different fluid (e.g. R-290) with lower capacity, evaluate what the evaporation and condensation would be for this R-22 unit at the (lower) capacity of R-290:
  - Correct the leaving air temperature at the condenser (Delta-T proportional to capacity)
  - Correct the LMTD's at evaporator and condenser (proportional to capacity) for the lower capacity.
  - Calculate the Carnot efficiencies at full and reduced capacity: COP<sub>Carnot</sub> = Te / (Tc – Te)
  - Assume the ratio [COP / COP<sub>Carnot</sub>] is the same at full and reduced capacity.
  - $\rightarrow$  Calculate the corrected COP at reduced capacity



# **Correction for cooling capacity (3)**

- Superimposed on results from AREP #62 report.
- The blue line represents what the COP would be with R-22 at variable cooling capacity.
- The blend alternatives to R-22 are even lower than before correction, because their capacity is lower.
- R-290 has slightly better COP than R-22, but not as much as it appears without correction.
- From cycle calculations, R-290 had slightly lower COP than R-22.



 The difference between measured R-290 and corrected R-22 is within measurement uncertainties, but may also come from factors not taken in the model: differences in heat transfer, pressure drops, compressor efficiency etc...

### Conclusions

- This study provided methods to:
  - Analyze the cycle efficiency of blends, accounting for variations in system configuration.
  - Cross-compare alternatives to R-22 and R-410A.
  - Correct the measured COP of various fluids according to their cooling capacity.
- Comparisons show (or confirm) that:
  - Blends are highly sensitive to system configuration.
  - Alternatives to R-410A do not match the COP of R-22.
  - R-290 has COP similar to or slightly better than R-22, but not so much better as from uncorrected measured data.



### **But Caution** !

- This is cycle calculation. A model cannot take everything into account.
- Legitimate questions can be raised about some assumptions. Must be kept in mind when looking at he results: • Constant in-tube heat transfer coefficients. the results:

  - Extreme" heat exchangers arrangements.
  - Constant compressor efficiency.
  - In HAT, same indoor conditions as AHRI.
- This contribution to analysis cannot replace further testing and optimization with various fluids, taking cost into account.



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#### **QUESTIONS?**

# Paul.delarference on Compressors and <u>Paul.delarference on Compressors and</u> The 8th Internation Refrigeration, 2017 Refrigeration, 2017

